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Simulation of natural convection with the Collocated Clustered Finite Volume scheme

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Abstract

This paper presents numerical results obtained in the case of natural convection within non constant fluid density, using the Collocated Clustered Finite Volume (CCFV) scheme. The continuous equations are first given in a dimensionless form. Then we present the finite volume scheme with the principles and the spatial discretization used. Analytical tests illustrate the numerical behavior of this scheme according to the type of grid, of the pressure stabilization method and check the robustness of this scheme. Next, the results obtained on the square thermally driven cavity under large temperature differences show that the CCFV scheme accurately fits the reference results.

1 Introduction

Various fluid flows are successfully modeled by the Navier-Stokes equations within the Oberbeck-Boussinesq approximation: the fluid properties are assumed to be constant in the mass, momentum and energy conservation equations, except in the buoyancy term where a linear dependence of the density with respect to the temperature is taken into account. This approximation is justified when the range of relative temperature variations is small enough (the mathematical validation of this approximation is examined in [1,2]), and then leads to a simpler mathematical formulation than the complete equations. However, when the temperature gap increases significantly, the variations of the fluid properties cannot be neglected.

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The Navier-Stokes and energy equations with variable fluid properties involve many non-linear terms, which have to be handled by numerical methods. Adaptations of the collocated finite volume schemes [3–5] to this case are often necessary in the engineering framework. In the Collocated Clustered Finite Volume method, the discrete unknowns are all located at the center of the cells of a unique mesh. Since the equivalent of the well-known “inf-sup” condition in the finite element setting (see [6]), or also called LBB condition (see [7]), is not satisfied by a collocated scheme, stabilization methods have to be implemented in order to avoid unrealistic pressure oscillations, sometimes called “checkerboard modes”. Among the pressure stabilization techniques, let us cite the Brezzi and Pitkaranta approach [8], first introduced in the framework of the finite element method, which consists in adding in the mass conservation equation a stabilization term proportional to the laplacian of the pressure. Another common pressure stabilization technique is the “Momentum interpolation Method”, presented by Rhie and Chow in [9] and usually practiced within the use of time stepping methods in finite difference or volume schemes.

We have introduced in [4,10] the Collocated Clustered Finite Volume (CCFV) scheme, presenting the following characteristics:

- (1) This scheme holds for a large class of grids, the only geometric requirement being that in every control volume, one can select a particular point, called the center of the control volume, such that each interface between two adjacent control volumes is orthogonal to the line joining their centers. This condition applies for rectangular or parallelepipedic meshes, triangular (2D) or tetrahedral (3D) Delaunay meshes, and Voronoï meshes.
- (2) The scheme is fully coupled, and the discrete gradient operator is defined as the adjoint of the discrete divergence operator, thus ensuring the decrease of the kinetic energy for incompressible and isothermal fluid flows. The discrete non-linear mass, momentum and energy equations are simultaneously solved using an under-relaxed Newton’s method, and the linear systems are solved using an iterative linear solver, namely the BiCGStab method preconditioned by an incomplete LU factorization.
- (3) The pressure stabilization method is performed by selecting clusters of control volumes, i.e. small sets of control volumes, such that a stabilization term is imposed in the equation of the mass conservation, only on the edges between neighboring control volumes belonging to the same cluster. This procedure allows keeping stable discrete solutions, while the approximate solution is shown to converge to a solution of the Navier-Stokes equations.

We present in this paper the extension of the CCFV scheme to non constant fluid properties, thus permitting to handle the low Mach number equations for large temperature variations. Note that this extension leads to several new difficulties:

- (1) New non-linear terms have to be handled.
- (2) Since the density is not constant, one has to account for cross derivative terms involved by the viscous stress tensor.
- (3) The thermodynamic pressure must be computed in agreement with the temperature field.

We take advantage in this paper of the fact that the CCFV is natively a non-linear coupled scheme, the extension of which the new non-linear terms appears to be straightforward. New developments, based of recent research results on finite volume methods [11] have allowed for accounting for cross derivative terms resulting from variable density.

The outlines of this paper are the following. We give in section 2 the fluid flow equations with non constant physical properties. In section 3 are presented the numerical scheme and the main features of its practical implementation. Numerical results are then described in section 4 showing some convergence properties, the effect of the pressure stabilization method and comparisons with a benchmark, and some conclusions are drawn in section 5.

2 Low Mach number approximation

The low Mach number model, suggested by Paolucci in the early 1980s [12], is used in studying very low velocity flows such as natural convection in a large temperature difference [13,14]. In this approach, the total pressure is the sum of a mean pressure $P^*(t)$ in the fluid domain Ω , called the thermodynamic pressure, and fluctuations of the pressure $p^*(\vec{x}^*, t^*)$, supposed to be such that $\int_{\Omega} p^*(\vec{x}^*, t^*) dv(\vec{x}^*) = 0$ for all time t^* . From now on, the dimensional quantities are labeled with $*$.

The dimensionless low Mach number equations for an ideal gas in an enclosure with impervious walls at the initial constant state (P_0^*, T_0^*) and under the gravitational force per mass unit $-g^* \vec{e}_z$ are:

$$\frac{\partial}{\partial t} \rho + \vec{\nabla} \cdot (\rho \vec{v}) = 0 \quad (1)$$

$$\frac{\partial}{\partial t} (\rho \vec{v}) + \vec{\nabla} \cdot (\rho \vec{v} \otimes \vec{v}) = -\vec{\nabla} p - \frac{RaPr}{\varepsilon_T} \rho \vec{e}_z + Pr \vec{\nabla} \cdot \bar{\bar{\tau}} \quad (2)$$

$$\frac{\partial}{\partial t} (\rho T) + \vec{\nabla} \cdot (\rho T \vec{v}) = \frac{\gamma - 1}{\varepsilon_T \gamma} \frac{dP}{dt} + \vec{\nabla} \cdot (k \vec{\nabla} T) \quad (3)$$

$$\int_{\Omega} \rho dv(\vec{x}) = \int_{\Omega} dv(\vec{x}), \quad \int_{\Omega} p(\vec{x}, t) dv(\vec{x}) = 0 \quad (4)$$

$\bar{\tau}$ represents the viscous stress tensor, that we assume to be given by the Stokes relation with $\bar{\mathbf{I}}$, the identity tensor:

$$\bar{\tau} = \mu \left(\vec{\nabla} \vec{v} + (\vec{\nabla} \vec{v})^t - \frac{2}{3} (\vec{\nabla} \cdot \vec{v}) \bar{\mathbf{I}} \right) \quad (5)$$

Notice that radiative fluxes are neglected in the energy equation and the diffusive heat flux is expressed using the Fourier law $\vec{q} = -k \vec{\nabla} T$. As ρ is supposed to verify the ideal gas law, we obtain:

$$\rho = \frac{P}{1 + \varepsilon_T T} \quad (6)$$

where ρ , \vec{v} , p , P , and T are respectively the non-dimensional density, velocity, spatially pressure fluctuations (often called dynamic pressure), thermodynamic pressure and temperature where $\rho = \rho^*/\rho_0^*$, $\vec{v} = \vec{v}^*/v_0^*$, $p = p^*/(\rho_0^* v_0^{*2})$, $P = P^*/P_0^*$ and $T = (T^* - T_0^*)/\Delta T^*$. The space variable \vec{x}^* and velocity have been normalized by the reference height H^* , and by the ratio between the thermal diffusivity at the reference state, a_0^* , and H^* . The dynamic viscosity and thermal conductivity are normalized by their reference values at (P_0^*, T_0^*) . Three dimensionless parameters appear in these equations: the Rayleigh number $Ra = (g^* H^{*3} \varepsilon_T)/(a_0^* \nu_0^*)$, the Prandtl number $Pr = \nu_0^*/a_0^*$ and the parameter $\varepsilon_T = \Delta T^*/T_0^*$.

The next section of the paper is devoted to the description of the discrete approximations of terms involving in the low Mach number model.

3 The Collocated Clustered Finite Volume scheme

We now intend to present the scheme for the approximation of a solution (P, p, T, \vec{v}) to system (1-3) with (4)-(6). Only the space discretization is presented with centered approximations. Upwind schemes and time discretization can be found in [4] and convergence proofs in [10].

In the following subsections, we first give definitions related to meshes, then we present the space discretization of system (1-3) and associated principles for this finite volume scheme.

3.1 Admissible meshes

The domain Ω is completely recovered by a family \mathcal{M} of unstructured convex polyhedra, called control volumes. The detailed notations for the geometric quantities involved by the discretization are illustrated in figure 1 in the 2d-case.

Let us introduce some notations: we denote by \mathcal{M} the set of all the control volumes. For each control volume K , we denote by \vec{x}_K the coordinates of its center, by $m(K)$ its area (if $d = 2$) or its volume (if $d = 3$), by \mathcal{N}_K the set composed by the neighbors of K . We denote by $\mathcal{E}_{K,\text{int}}$ the set of the internal edges and by $\mathcal{E}_{K,\text{ext}}$, the set of the external edges. If the control volume L is a neighbor of the control volume K , we denote by $m(\sigma_{KL})$ the length ($d = 2$) or the area ($d = 3$) of the interface σ_{KL} between K and L ($\sigma_{KL} \in \mathcal{E}_{K,\text{int}}$). If the control volume K has an edge σ at the boundary domain ($\sigma \in \mathcal{E}_{K,\text{ext}}$), we denote by $m(\sigma)$ the length ($d = 2$) or the area ($d = 3$) of the interface σ at the boundary. We denote by \vec{x}_σ the orthogonal projection of \vec{x}_K on σ , by $\vec{n}_{K,\sigma}$ the unit vector normal to σ , outward of K , and by $d_{K,\sigma}$, the distance between \vec{x}_K and \vec{x}_σ . We then denote by $\vec{x}_{K\sigma}$ the center of gravity of the interface σ .

The main objective to elaborate this numerical scheme was its simplicity, in particular for the expression of diffusion fluxes. So the approximation of the flux normal to the edge of a control volume σ_{KL} depends only on two adjacent cells what permits to systematically satisfy monotonic solutions for diffusive equations. To allow it, the requirements to mesh the domain are:

$$\sigma_{KL} \perp \overrightarrow{x_K x_L} \tag{7}$$

$$\overrightarrow{x_K x_L} \cdot \vec{n}_{KL} > 0 \tag{8}$$

From (7), we get the orthogonality property whereas relation (8) defines the order of the cell center occurrence in the direction of \vec{n}_{KL} . These conditions are checked for rectangular or parallelepiped and dual Delaunay-Voronoi grids. Recall that a Voronoi mesh is such as the control volume K is as the set of points closer to \vec{x}_K than to any other \vec{x}_L . Therefore, the edge separating cells K and L belongs to the mid-plan between \vec{x}_K and \vec{x}_L what implies that requirements (7) and (8) are automatically checked. For triangular (2d) or tetrahedral (3d) grids, the center \vec{x}_K of the cell K is the circumcenter (condition (7)); the constraint (8) is automatically verified once the Delaunay criterion is satisfied.

3.2 Spatial discretization of the Navier-Stokes and energy equations

The objective in the development of this numerical scheme is that solutions of the discrete Navier-Stokes and energy equations p_K, \vec{v}_K, T_K , accurately approximate p, \vec{v}, T at the point \vec{x}_K of each control volume $K \in \mathcal{M}$. Our discrete spatial operators are also constructed so that, by multiplying the momentum and the thermal equations expressed on cell K with the velocity \vec{v}_K and the temperature T_K , and by summing over all the cells, we recover discrete approximations of the kinetic and thermal energy balances. For example, the works of the pressure forces and of the non-linear inertial forces must vanish under Boussinesq approximation.

For the sake of clarity, the discrete spatial operators are presented for enclosures with impervious walls and only for Dirichlet boundary conditions. The following notations are used in the next sections. We denote by $(A(\vec{x}))_D$ the discrete approximation of the continuous form $A(\vec{x})$ and by $(A(\vec{x}))_{D,K}$ the discrete approximation evaluated at the cell center \vec{x}_K ; $v^{(i)}$ is the i -th component of the velocity vector \vec{v} and ∂_i marks out the partial derivative into the i -th direction.

3.2.1 Mass equation

Let us first give the approximation of the steady mass equation integrated over the cell K , $\int_K \vec{\nabla} \cdot (\rho \vec{v}) dv(\vec{x})$ that is:

$$m(K) \left(\vec{\nabla} \cdot (\rho \vec{v}) \right)_{D,K} = \sum_{L \in \mathcal{N}_K} F_{KL} \quad (9)$$

where F_{KL} is the approximation of the mass flux $\mathcal{F}_{KL} = \int_{\sigma_{KL}} \rho \vec{v}(\vec{x}) \cdot \vec{n}_{KL} ds(\vec{x})$ between two neighboring control volumes K and L . Notice that no boundary contribution is introduced because of the impervious walls.

To preserve a good coupling between pressure and velocity, the approximation of the velocity crossing the edges σ_{KL} must be second order accurate at the gravity center of the face [15]. This condition is easily fulfilled by using a linear interpolation of the velocity $\vec{v}(\vec{x}_{KL}) = \sum_{I \in \mathcal{M}} \alpha_I \vec{v}(\vec{x}_I)$. Practically, nodes \vec{x}_K and \vec{x}_L are involved plus, eventually, one or two other nodes close to \vec{x}_{KL} .

Without any loss of generality, we now suppose that only centers \vec{x}_K and \vec{x}_L play a part in the interpolation. This case corresponds to a mesh where the intersection point between the line (\vec{x}_K, \vec{x}_L) and the edge σ_{KL} is exactly \vec{x}_{KL} , the gravity center of the face σ_{KL} . Parallelepipeds in 3d [4] or rectangles and Delaunay triangles in 2d satisfy these requirements. The discrete mass flux

then writes:

$$F_{KL} = \rho_{KL} \left(m(\sigma_{KL})(a_{KL}\vec{v}_K + a_{LK}\vec{v}_L) \cdot \vec{n}_{KL} - \lambda_{KL} \frac{m(\sigma_{KL})}{d_{KL}} (p_L - p_K) \right) \quad (10)$$

with

$$a_{KL} = \frac{\overline{x_{KL}x_L} \cdot \vec{n}_{KL}}{d_{KL}}, \quad a_{KL} + a_{LK} = 1$$

The density ρ_{KL} on interface σ_{KL} is also evaluated with a linear interpolation.

A stabilization method is necessary to prevent from the apparition of pressure oscillations in collocated schemes. We use the method presented in [4] that consists in modifying the mass equation by introducing a stabilization contribution which corresponds to the second term of the right-hand-side of equation (10), where λ_{KL} is a stabilization parameter defined on each interface between two control volumes K and L .

Recall briefly the principle of pressure stabilization method. The family of control volumes \mathcal{M} is partitioned into disjoint subsets including groups of neighboring control volumes, with any algorithm ensuring that two control volumes belonging to the same subset are not too distant one from each other (Fig.2). An example of such an algorithm can be found in [4].

Then λ_{KL} is chosen according to the following rule:

- $\lambda_{KL} = \lambda$ for any pair of neighboring control volumes K and L belonging to the same subset,
- $\lambda_{KL} = 0$ otherwise.

The value λ is a positive value, chosen large enough for preventing from the apparition of instabilities. The main advantage of gathering the cells by clusters is that the mass redistribution due to the stabilization term is limited to each cluster.

3.2.2 Transport terms

For $\phi \in \{v^{(i)}, T\}$, the discrete expression of the non-linear term integrated over the cell K is:

$$m(K) \left(\vec{\nabla} \cdot (\rho \vec{v} \phi) \right)_{D,K} = \sum_{L \in \mathcal{N}_K} G_{KL} \quad (11)$$

where G_{KL} is the approximation of the flux $\mathcal{G}_{KL} = \int_{\sigma_{KL}} (\rho \vec{v}(\vec{x}) \cdot \vec{n}_{KL}) \phi(\vec{x}) ds(\vec{x})$. To satisfy the discrete kinetic and thermal energy balances, the transport velocity must be equal to the discrete mass flux crossing each edge (Eq. (10)) and the centered approximation of ϕ must be used:

$$G_{KL} = F_{KL} \frac{\phi_K + \phi_L}{2}$$

By taking into account the mass equation for a steady flow, $\sum_{L \in \mathcal{N}_K} F_{KL} = 0$, relation (11) also writes:

$$m(K) \left(\vec{\nabla} \cdot (\rho \vec{v} \phi) \right)_{D,K} = \sum_{L \in \mathcal{N}_K} F_{KL} \frac{\phi_L - \phi_K}{2}$$

3.2.3 Pressure

The discrete approximation of the pressure gradient is based on its duality with the discrete velocity divergence:

$$\sum_{K \in \mathcal{M}} m(K) \left(\vec{v}_K \cdot (\vec{\nabla} p)_{D,K} \right) = - \sum_{K \in \mathcal{M}} \left[\left(\sum_{L \in \mathcal{N}_K} m(\sigma_{KL}) (a_{KL} \vec{v}_K + a_{LK} \vec{v}_L) \vec{n}_{KL} \right) p_K \right]$$

Thus we obtain

$$m(K) (\vec{\nabla} p)_{D,K} = \sum_{L \in \mathcal{N}_K} m(\sigma_{KL}) a_{KL} (p_L - p_K) \vec{n}_{KL} \quad (12)$$

By using the geometric property $\sum_{L \in \mathcal{N}_K} m(\sigma_{KL}) \vec{n}_{KL} + \sum_{\sigma \in \mathcal{E}_{K,\text{ext}}} m(\sigma) \vec{n}_{K,\sigma} = 0$, another form for the pressure gradient can be established:

$$m(K) (\vec{\nabla} p)_{D,K} = \sum_{L \in \mathcal{N}_K} m(\sigma_{KL}) (a_{KL} p_L + a_{LK} p_K) \vec{n}_{KL} + \sum_{\sigma \in \mathcal{E}_{K,\text{ext}}} m(\sigma) p_K \vec{n}_{K,\sigma} \quad (13)$$

Notice that relations (12) and (13) do not provide consistent approximations of the equivalent forms $\int_K \vec{\nabla} p \, dv(\vec{x})$ and $\int_{\delta_K} p \, \vec{n} ds(\vec{x})$, except when $a_{KL} = 0.5$.

3.2.4 Viscous diffusion

In the low Mach number model, the viscous term integrated over the cell K writes:

$$\begin{aligned} \int_K \vec{\nabla} \cdot \bar{\tau} \, dv(\vec{x}) &= \int_K \vec{\nabla} \cdot (\mu \vec{\nabla} \vec{v}) \, dv(\vec{x}) + \int_K \vec{\nabla} \cdot (\mu \vec{\nabla}^t \vec{v}) \, dv(\vec{x}) - \frac{2}{3} \int_K \vec{\nabla} \cdot (\mu \vec{\nabla} \cdot \vec{v}) \, dv(\vec{x}) \\ &= \int_K \vec{a}(\mu, \vec{v}) \, dv(\vec{x}) + \int_K \vec{b}(\mu, \vec{v}) \, dv(\vec{x}) - \frac{2}{3} \int_K \vec{c}(\mu, \vec{v}) \, dv(\vec{x}) \end{aligned}$$

Let us now give the approximations of these three integrals.

- The approximation of $\vec{a}(\mu, \vec{v})$ is:

$$m(K)(\vec{a}(\mu, \vec{v}))_{D,K} = \sum_{L \in \mathcal{N}_K} \vec{A}_{KL} + \sum_{\sigma \in \mathcal{E}_{K,\text{ext}}} \vec{A}_{K,\sigma} \quad (14)$$

where \vec{A}_{KL} and $\vec{A}_{K,\sigma}$ are the approximations of $\vec{\mathcal{A}}_{KL} = \int_{\sigma_{KL}} \vec{\nabla} \vec{v}(\vec{x}) \cdot \vec{n}_{KL} ds(\vec{x})$ and $\vec{\mathcal{A}}_{K,\sigma} = \int_{\sigma} \vec{\nabla} \vec{v}(\vec{x}) \cdot \vec{n}_{K,\sigma} ds(\vec{x})$. Thanks to the mesh properties (7) and (8), we simply obtain:

$$\vec{A}_{KL} = \mu_{KL} \frac{m(\sigma_{KL})}{d_{KL}} (\vec{v}_L - \vec{v}_K) \text{ and } \vec{A}_{K,\sigma} = \mu_{\sigma} \frac{m(\sigma)}{d_{K,\sigma}} (\vec{v}_{\sigma} - \vec{v}_K) \quad (15)$$

where \vec{v}_{σ} is the approximation of $\vec{v}(\vec{x}_{\sigma})$, μ_{KL} and μ_{σ} are the dynamic viscosity computed on edges.

- The discrete contribution $\int_K \vec{b}(\mu, \vec{v}) \, dv(\vec{x})$ is achieved by considering the weak form:

$$\sum_{i=1}^d \int_{\Omega} u^{(j)} \partial_i (\mu \partial_j v^{(i)}) dv(\vec{x}) = - \sum_{i=1}^d \int_{\Omega} \partial_i u^{(j)} \mu \partial_j v^{(i)} dv(\vec{x}) \quad (16)$$

with $u^{(j)}$ the j -th component of a vectoriel test function \vec{u} , $u^{(j)}$ being null on Dirichlet boundary conditions. By using the i -th component of the discrete strong gradient expression $(\partial_i \phi)_{D,K}$ [11],

$$\begin{aligned} (\partial_i \phi)_{D,K} &= \frac{1}{m(K)} \left(\sum_{L \in \mathcal{N}_K} \frac{m(\sigma_{KL})}{d_{KL}} (\phi_L - \phi_K) (x_{KL}^{(i)} - x_K^{(i)}) + \right. \\ &\quad \left. \sum_{\sigma \in \mathcal{E}_{\text{ext}}} \frac{m(\sigma)}{d_{K,\sigma}} (\phi_{\sigma} - \phi_K) (x_{K\sigma}^{(i)} - x_K^{(i)}) \right) \end{aligned} \quad (17)$$

the discretization of the right-hand-side of (Eq. 16) writes:

$$\left(\sum_{i=1}^d \int_{\Omega} \mu \partial_i u^{(j)} \partial_j v^{(i)} dv(\vec{x}) \right)_D = \sum_{i=1}^d \sum_{K \in \mathcal{M}} m(K) \mu_K (\partial_i u^{(j)})_{D,K} (\partial_j v^{(i)})_{D,K}$$

The k-th component of the discrete contribution of $\int_K \vec{b}(\mu, \vec{v}) dv(\vec{x})$ is obtained by substituting $(\partial_i u^{(j)})_{D,K}$ and $(\partial_j v^{(i)})_{D,K}$ by the expressions (17) for $\phi = u^{(j)}$ and $\phi = v^{(i)}$ and by choosing the test function $u_L^{(j)} = \delta_{KL} \delta_{jk}$:

$$m(K)(b^{(k)}(\mu, \vec{v}))_{D,K} = \sum_{L \in \mathcal{N}_K} B_{KL}^{(k)} + \sum_{\sigma \in \mathcal{E}_{K,\text{ext}}} B_{K,\sigma}^{(k)} \quad (18)$$

with

$$B_{KL}^{(k)} = \frac{m(\sigma_{KL})}{d_{KL}} \sum_{i=1}^d \left(\mu_K (\partial_k v^{(i)})_{D,K} (x_{KL}^{(i)} - x_K^{(i)}) + \mu_L (\partial_k v^{(i)})_{D,L} (x_L^{(i)} - x_{KL}^{(i)}) \right)$$

$$B_{K,\sigma}^{(k)} = \frac{m(\sigma)}{d_{K,\sigma}} \sum_{i=1}^d \left(\mu_K (\partial_k v^{(i)})_{D,K} (x_{K\sigma}^{(i)} - x_K^{(i)}) + \mu_L (\partial_k v^{(i)})_{D,L} (x_L^{(i)} - x_{L\sigma}^{(i)}) \right)$$

- The k-th component of discrete contribution of $\int_K \vec{c}(\mu, \vec{v}) dv(\vec{x})$ writes:

$$m(K)(c^{(k)}(\mu, \vec{v}))_{D,K} = \sum_{L \in \mathcal{N}_K} C_{KL}^{(k)} + \sum_{\sigma \in \mathcal{E}_{K,\text{ext}}} C_{K,\sigma}^{(k)} \quad (19)$$

with

$$C_{KL}^{(k)} = \frac{m(\sigma_{KL})}{d_{KL}} \sum_{i=1}^d \mu_K (\partial_i v^{(i)})_{D,K} (x_{KL}^{(k)} - x_K^{(k)}) + \frac{m(\sigma_{KL})}{d_{KL}} \sum_{i=1}^d \mu_L (\partial_i v^{(i)})_{D,L} (x_L^{(k)} - x_{KL}^{(k)})$$

$$C_{K,\sigma}^{(k)} = \frac{m(\sigma)}{d_{K,\sigma}} \sum_{i=1}^d \mu_K (\partial_i v^{(i)})_{D,K} (x_{K\sigma}^{(k)} - x_K^{(k)}) + \frac{m(\sigma)}{d_{K,\sigma}} \sum_{i=1}^d \mu_L (\partial_i v^{(i)})_{D,L} (x_L^{(k)} - x_{L\sigma}^{(k)})$$

Note that the use of the strong gradient (17) in $\int_K \vec{a}(\mu, \vec{v}) dv(\vec{x})$ may give rise to numerical instabilities. Therefore, to prevent from these oscillations, relation (14) must absolutely be applied instead.

3.2.5 Thermal diffusion

In the energy equation, the discrete contribution $(h(k, T))_{D,K}$ provided by the approximation of the diffusion term $\int_K h(k, T) dv(\vec{x}) = \int_K \vec{\nabla} \cdot (k \vec{\nabla} T) dv(\vec{x})$ is similar to relations (14) with (15):

$$m(K)(h(k, T))_{D,K} = \sum_{L \in \mathcal{N}_K} H_{KL} + \sum_{\sigma \in \mathcal{E}_{K,\text{ext}}} H_{K,\sigma}$$

The approximations H_{KL} and $H_{K,\sigma}$ of the conducted heat fluxes on σ_{KL} , $\mathcal{H}_{KL} = \int_{\sigma_{KL}} k \vec{\nabla} T(\vec{x}) \cdot \vec{n}_{KL} ds(\vec{x})$, and on σ , $\mathcal{H}_{K,\sigma} = \int_{\sigma} k \vec{\nabla} T(\vec{x}) \cdot \vec{n}_{K,\sigma} ds(\vec{x})$, write:

$$H_{KL} = k_{KL} \frac{m(\sigma_{KL})}{d_{KL}} (T_L - T_K) \text{ and } H_{K,\sigma} = k_\sigma \frac{m(\sigma)}{d_{K,\sigma}} (T_\sigma - T_K)$$

where T_σ is the approximation of $T(\vec{x}_\sigma)$, k_{KL} and k_σ are thermal conductivities on σ_{KL} and σ .

3.3 Discrete equations and solvers

We get a system of non-linear equations, which depends on the unknowns of the control volume K itself, on the unknowns of the neighbors $L \in \mathcal{N}_K$ of K or on boundary $\sigma \in \mathcal{E}_{K,\text{ext}}$, and also, because of $(\vec{b}(\mu, \vec{v}))_D$ and $(\vec{c}(\mu, \vec{v}))_D$ exist, on unknowns of the neighbors $M \in \mathcal{N}_L$ of L . Note that under the Boussinesq approximation, the mass equation $\vec{\nabla} \cdot \vec{v} = 0$ implies $\vec{c}(\mu, \vec{v}) = \vec{0}$ and if furthermore the viscosity is constant, $\vec{b}(\mu, \vec{v}) = \vec{0}$. In that case, the equation on cell K only depends on its neighbors $L \in \mathcal{N}_K$ or on boundary $\sigma \in \mathcal{E}_{K,\text{ext}}$.

In our implementation, the non-linear system is solved using an under-relaxed Newton method. The resulting linear equations are then solved by an iterative linear solver using the BiCGStab method preconditioned by an incomplete LU factorization, with variable fill-in levels (a detailed description can be found in [4]). The thermodynamic pressure P is then updated at the end of each Newton iteration, solving the discrete form of the total mass conservation equation given in (4).

4 Natural convection results

The computational domain is meshed either by rectangular cells or by Delaunay triangles thanks to a free software developed by Saltel and Hecht [16].

4.1 Analytical tests

We consider the stationary fluid flow and heat transfer in a square cavity with a low Mach number model. The dimensionless velocity, pressures, density and temperature fields are solutions of equations (1-6) where the time derivatives are zero. No-slip boundary conditions are applied on the isothermal walls.

To study the accuracy of the numerical method in the non-Boussinesq regime, forcing terms are added in the momentum and energy equations in order to converge towards the prescribed solution:

$$\begin{aligned}
P &= 1 \\
T &= \sin^2(\pi x^{(1)}) \sin^2(\pi x^{(2)}) \\
\rho &= \frac{P}{1 + \varepsilon_T T} \\
p &= \sin^2(\pi x^{(1)}) \sin^2(\pi x^{(2)}) \\
v^{(1)} &= \frac{\partial \Psi}{\partial x^{(2)}} = 2\pi \cos(\pi x^{(2)}) \sin(\pi x^{(2)}) \sin^2(\pi x^{(1)}) \\
v^{(2)} &= -\frac{\partial \Psi}{\partial x^{(1)}} = -2\pi \cos(\pi x^{(1)}) \sin(\pi x^{(1)}) \sin^2(\pi x^{(2)})
\end{aligned}$$

The velocity and the density (i.e. the temperature) are chosen so that $\vec{\nabla} \cdot (\rho \vec{v}) = 0$. Sutherland laws are used to evaluate the dimensionless dynamical viscosity as a function of the temperature:

$$\mu = (\varepsilon_T T + 1)^{3/2} \left(\frac{1 + S^*/T_0^*}{1 + \varepsilon_T T + S^*/T_0^*} \right) \quad (20)$$

where $S^* = 110.5 K$ is the *Sutherland constant*. The variation laws of the thermal conductivity k and dynamical viscosity μ , as a function of the temperature, are supposed identical, and computations are carried out with $Ra = 1$ and $Pr = 1$. The deviation from the analytical solution is measured by the discrete L_2 -norm:

$$\|e(\phi)\|_2^2 = \sum_{K \in \mathcal{M}} m(K) (\phi_K - \phi(\vec{x}_K))^2, \quad \phi \in \{v^{(i)}, T, p, \rho\}$$

4.1.1 Spatial accuracy

Figures 3a-3d show the L_2 -norm of errors between the analytical and numerical solutions as a function of mean mesh size $h = 1/\sqrt{N}$, N being the number of triangles, and with three reduced temperature differences, $\varepsilon_T \in \{0, 1, 2\}$. Remark that the Boussinesq approximation is recovered when $\varepsilon_T = 0$. For all ε_T , the velocity, temperature and density are second-order accurate whereas the pressure is, like most of collocated schemes, first-order accurate only.

4.1.2 Comparison of pressure stabilization methods

The simulations are performed for the Boussinesq model, namely with $\varepsilon_T = 0$, and for Delaunay triangular meshes. Our pressure stabilization method, described in section 3.2.1, is compared with two other methods.

- The Brezzi and Pitkaranta method (BP) [8] consists in introducing a stabilization contribution $\lambda h^\alpha (\Delta p)_D$ in the mass equation, where $\alpha \in]0, 2[$,

h is the characteristic mesh size, $\alpha \in \mathfrak{R}$ is a positive small value and $\Delta_D p \equiv a_D(1, p)$ is the discrete laplacian operator applied on pressure and defined by (14):

$$(\vec{\nabla} \cdot \vec{v})_D = \lambda h^\alpha (\Delta p)_D$$

- The Rhie and Chow interpolation method (RC) [9] can also be viewed as a penalization technique of the mass equation:

$$(\vec{\nabla} \cdot \vec{v})_D = \lambda \left((\Delta p)_D - \left(\vec{\nabla} \cdot (\vec{\nabla} p)_D \right)_D \right)$$

where the second term of the right-hand-side is constructed with the strong gradient (17).

In figures 4a-4b are drawn the velocity and pressure errors as a function of λh^α , for three pressure stabilization techniques and for a mesh size $h = 0.019$. The accuracy of the all solutions decreases if the coefficient λh^α is too small: the pressure stabilization is insufficient and oscillations appear. For large coefficients, the errors for the velocity and pressure increase except when the stabilization is based on clusters. Our clusterization technique is very few sensitive to λh^α but the (RC)-method seems to provide more accurate pressure solutions for a wide gap of the coefficient.

Figures 5a-5d illustrate the convergence properties of these methods as a function of h and for two coefficients, $\lambda \in \{1, 0.0001\}$. For $\lambda = 1$, the slopes of the curve for the (BP)-method become worse, less than 2 and 1 for the velocity and pressure respectively. No significant difference distinguishes the convergence behavior of the cluster and (RC)- methods. The advantage of the cluster stabilization method with respect to the Rhie and Chow technique stems from the stability property of the resulting scheme. While the clusters and (BP)- methods introduce stable contributions in the discrete scheme and thus provide a L_2 stability for unsteady isothermal solutions [4,10,17,18], no such property can easily be proved for the (RC)-method because of the negative contribution $-\left(\vec{\nabla} \cdot (\vec{\nabla} p)_D\right)_D$ in the mass equation.

4.2 Benchmark comparisons

We consider the problem handled in the benchmark [19], stated in the above dimensionless form, which concerns the natural convection flow in a differentially heated square cavity. The vertical walls are isothermal at the uniform temperatures $T(0, y) = T_h = 1/2$ and $T(1, y) = T_c = -1/2$ with $0 \leq y \leq 1$, and the bottom and top boundaries are adiabatic. The ratio ε_T is given and equal to 1.2, and therefore the Boussinesq approximation no longer holds. The other dimensionless numbers are $\text{Pr} = 0.71$, $\gamma = 1.4$, $\text{Ra} = 10^6$ or $\text{Ra} = 10^7$. As in [19], we use the Sutherland law (Eq. 20) for the viscosity and assume

$\mu(T)/k(T)$ constant, which leads to a similar law for the thermal conductivity. We recall the definition of the local, $\text{Nu}(\vec{x})$, and average, $\widehat{\text{Nu}}_x$, Nusselt numbers:

$$\text{Nu}(\vec{x}) = k(T(\vec{x}))\vec{\nabla}T(\vec{x}) \cdot \vec{n}_{\partial\Omega}(\vec{x}) \text{ and } \widehat{\text{Nu}}_x = \int_0^1 \text{Nu}(\vec{x})dy,$$

The computations were performed either on a non-uniform distribution of Delaunay triangles or on different orthogonal grids where the sides of the rectangular control volumes follow a sinusoidal law in each direction to accurately represent the boundary layers. The stabilization parameter is equal to $\lambda = 10^{-6}$ and the iLU preconditioning is based on a three levels of fill-in.

4.2.1 Rayleigh number 10^6

In Table 1 are indicated the relative errors, with respect to solutions obtained with our scheme with a 304×304 rectangular grid, for the results computed on Delaunay triangles and drawn from [19]. Relative differences of benchmark solutions being smaller than 1%, our reference result is in good agreement with the literature. Bold underlines values smaller than 0.005% and show the good agreement with Vierendeels's results. The accuracy of results obtained with Delaunay triangular cells are good, except for the Nusselt number along the cold wall, $\max_y(\text{Nu}(1; y))$ and $\min_y(\text{Nu}(1; y))$. For non-Boussinesq flow model, the boundary layer along the cold wall is thicker than it is along the hot wall. The mesh size used being identical along the two vertical walls, it was therefore obvious that the accuracy of the heat transfer will be worst on the cold surface. The minima of the Nusselt number value are also larger than their corresponding maxima. The explanation is due to the fact that the coordinates, where $\min_y(\text{Nu}(0; y))$ and $\min_y(\text{Nu}(1; y))$ occur, are very close to the horizontal walls where a finer mesh should be desirable too.

The effect of the mesh size was also studied but it is not presented in this paper. Quadratic convergence has successfully been checked for the set of results except for minimal values of the Nusselt number when triangular meshes were considered.

4.2.2 Rayleigh number $Ra = 10^7$

For $Ra = 10^7$, only results obtained with rectangular grid are shown, the computational cost to solve the Navier-Stokes and energy equations on a fine enough triangular grid was judged too expensive. As shown in Table 2, our results are in excellent agreement with benchmark solutions [19]. Relative differences less than 0.005% are anew exhibited in bold. As for $Ra = 10^6$, the

second order accuracy of the scheme was successfully checked for the set of results.

5 Conclusion

Extension of the Collocated Clustered Finite Volume scheme to the low Mach number model was presented in detail. Convergence property of the new scheme was checked by considering an analytical solution. Effect of the pressure stabilization method was studied with respect to other stabilization techniques. Applications to natural convection problems with large temperature differences have led to results which are in good agreement with the literature.

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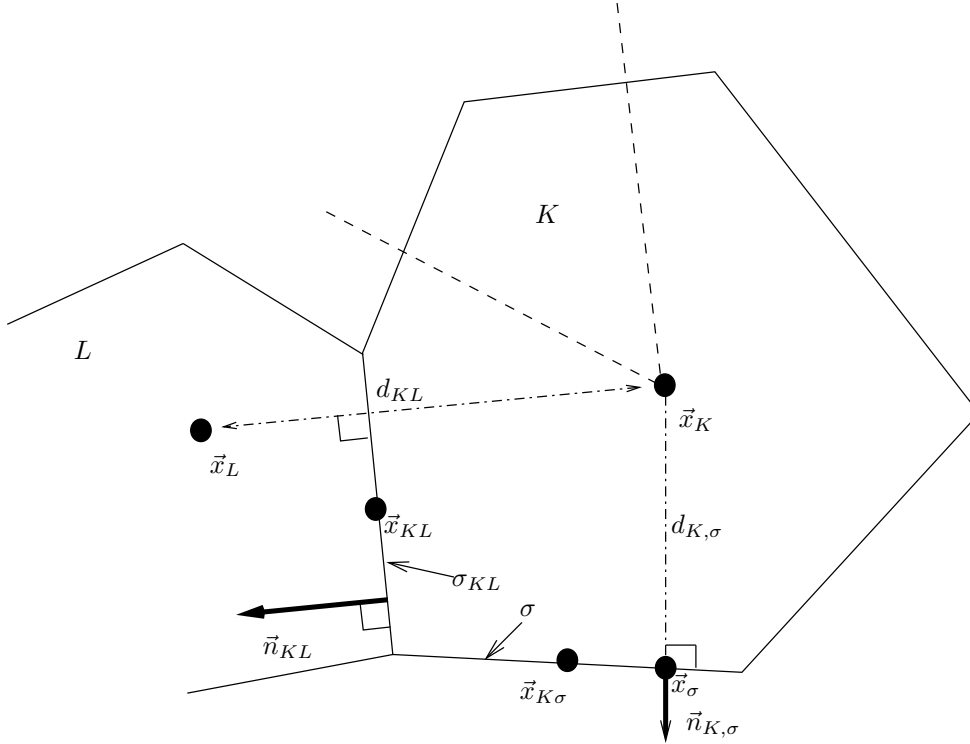
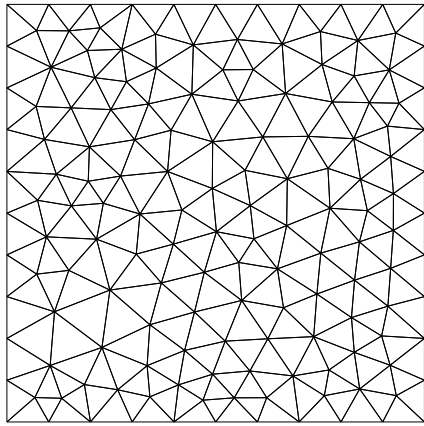
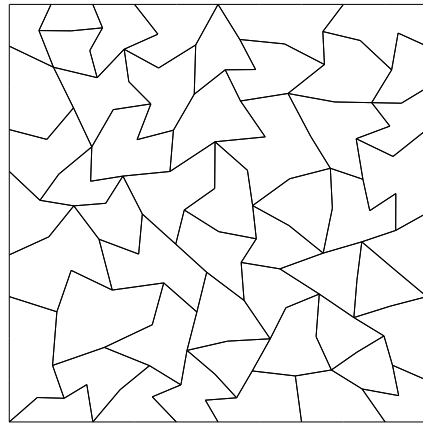


Fig. 1. Two neighboring control volumes K and L . One assumes that for all control volume K there exists a point denoted by \vec{x}_K in K such that, for any neighbor L of K , the straight line (\vec{x}_K, \vec{x}_L) is orthogonal to the common edge σ_{KL} . Then the length between \vec{x}_K and \vec{x}_L is denoted by d_{KL} , and the unit vector, normal to σ_{KL} and outward to K , is denoted by \vec{n}_{KL} . We then denote the center of gravity of the interface σ_{KL} by \vec{x}_{KL} . Similar notations are used when an edge σ belongs to $\delta\Omega$, the boundary of the domain Ω .



(a) Delaunay grid



(b) Clusters

Fig. 2. Delaunay grid and associated clusters

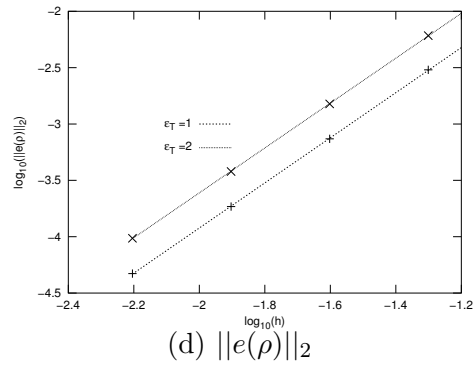
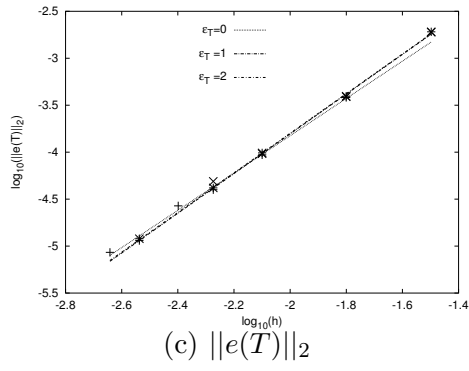
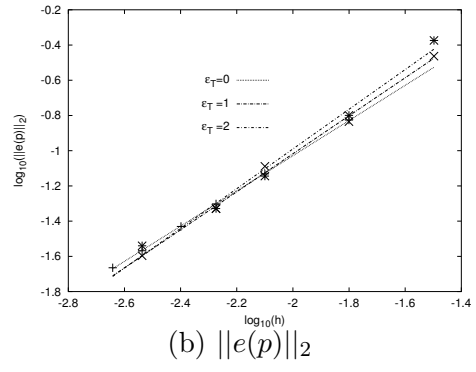
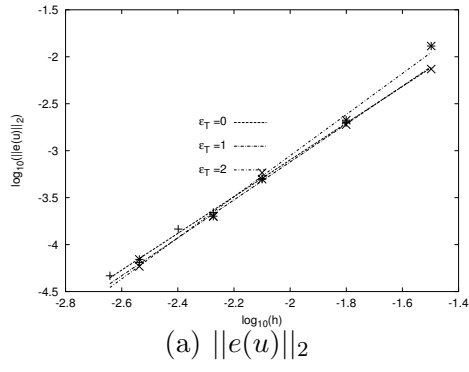


Fig. 3. Spatial accuracy for velocity, pressure, temperature and density

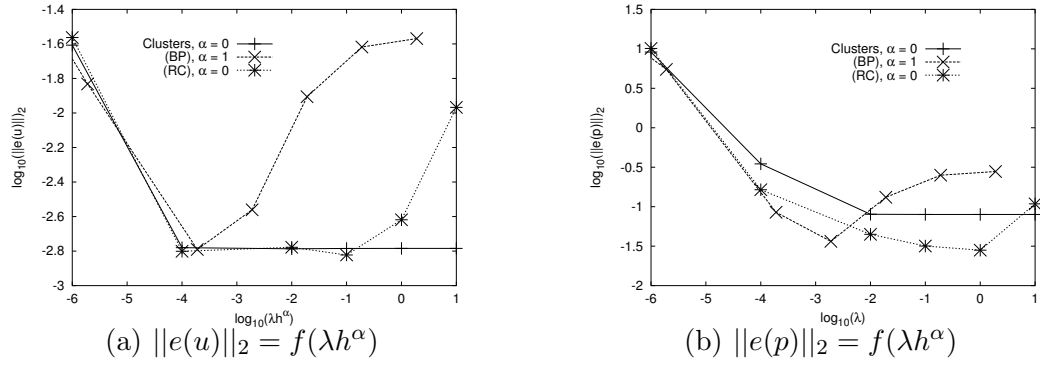


Fig. 4. Effect of the stabilization parameter λh^α on the L_2 -norm of the velocity and pressure, $\alpha = 0$ for the cluster method and the Rhie and Chow technique, (RC), whereas $\alpha = 1$ for the Brezzi and Pitkaranta method, (BP).

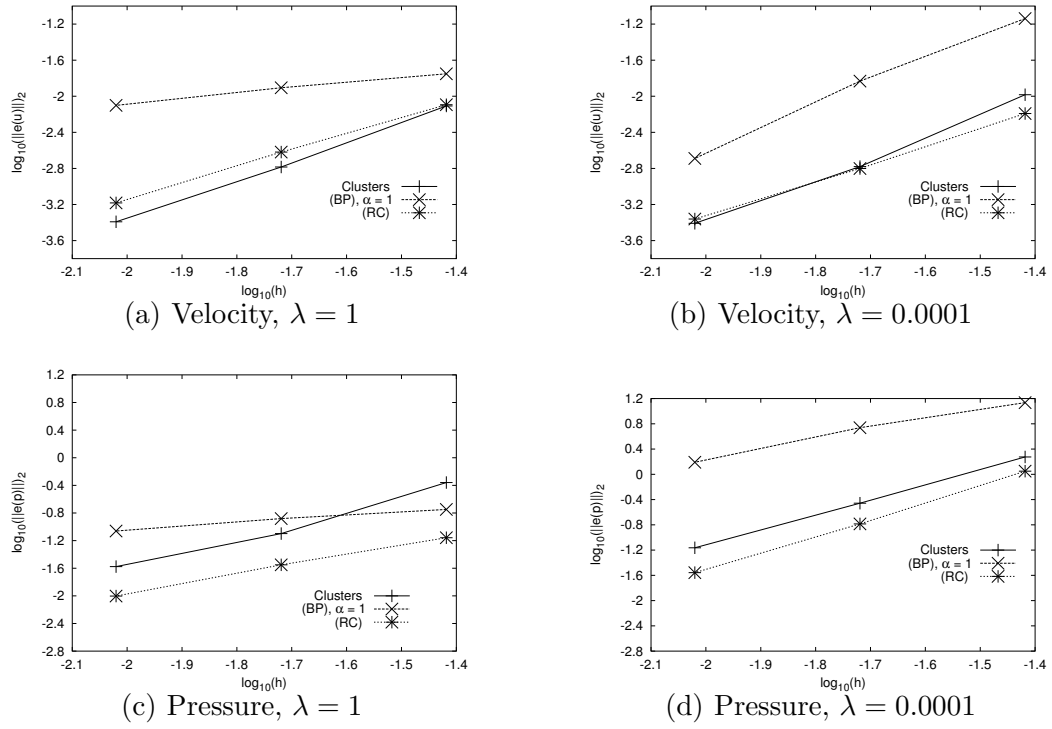


Fig. 5. Velocity and pressure errors as a function of h and λ for the cluster, Rhie and Chow (RC) and Brezzi and Pitkaranta (BP) methods.

	Vierendeels	Dabbene	Beccantini	Kloczko	Heuveline	Our results Triangular grid	Our results Rectangular grid
\widehat{Nu}_0	0.0012%	0.056%	0.0012%	0.099%	0.025%	0.027%	8.6867
\widehat{Nu}_1	0.0012%	0.014%	0.14%	0.61%	0.007%	0.027%	8.6867
Nu(0.0.5)	0.0013%	0.054%	0.016%	0.055%	N.A	0.05%	7.4592
Nu(1.0.5)	0.002%	0.25%	0.024%	0.55%	N.A	0.07%	8.6370
$\max_y(\text{Nu}(0;y))$	0.016%	0.18%	0.032%	0.24%	0.15%	0.01%	20.2737
$\min_y(\text{Nu}(0;y))$	0.028%	0.64%	0%	0.019%	0.037%	0.15%	1.0670
$\max_y(\text{Nu}(1;y))$	0.014%	0.34%	0.25%	0.91%	0.093%	0.45%	15.5216
$\min_y(\text{Nu}(1;y))$	0.040%	0.34%	0.052%	0.26%	0.15%	1%	0.7578
P	0.00075%	0.11%	0.0019%	0.034%	0.045%	0.02%	0.924482
Structured grid	2048×2048	320×320	169×148	160×160			304×304
Number of cells	4.2×10^6	102,400	25,012	25,600	200,000	173,030	92,416

Table 1
Comparison with results given in [19] for $Ra = 10^6$

	Vierendeels	Dabbene	Kloczko	Heuveline	Our results
\widehat{Nu}_0	0.0%	0.086%	0.38%	0.006%	16.2409
\widehat{Nu}_1	0.0%	0.32%	0.050%	0.10%	16.2409
$Nu(0, 0.5)$	0.0%	2.6%	0.068%	N.A	13.1886
$Nu(1, 0.5)$	0.0064%	1.6%	0.87%	N.A	15.5113
$\max_y(Nu(0, y))$	0.03%	0.31%	1.3%	0.15%	46.3941
$\min_y(Nu(0, y))$	0.068%	0.068%	1%	0.0%	1.45475
$\max_y(Nu(1, y))$	0.032%	1.0%	0.38%	0.35%	34.2832
$\min_y(Nu(1, y))$	0.0%	0.09%	2.8%	0.09%	1.08878
P	0.003%	0.04%	0.04%	0.04%	0.92261
Structured grid	2048×2048	160×160	100×100		304×304
Number of cells	4.2×10^6	25,600	10,000	400,000	92,416

Table 2
Comparison with results given in [19] for $Ra = 10^7$